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1 Exploring the Dual Dynamic Synergy of

² Transesterification and Siloxane Exchange in

3 Vitrimers

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13 ABSTRACT

14

Despite the benefits of dynamic polymer networks with multiple dynamic bonds, identifying compatible combinations of dynamic chemistries that work synergistically to achieve desirable properties remains a significant challenge. This work focuses on the potential of utilizing both siloxane and ester dynamic bonds in epoxy-acid cured vitrimers to finetune chemical exchange

19 reactions. We identified to what extent a common basic catalyst (TBD) can simultaneously 20 activate siloxane and ester exchange in the corresponding epoxy-based vitrimers. Our results 21 showed that TBD is not only able to facilitate network formation but also improved the dynamic 22 behavior of the resulting networks dramatically, with an overall exchange rate that is faster than 23 the sum of the individual exchange chemistries, as shown by stress-relaxation studies. It has been 24 demonstrated that the siloxane and ester dynamic bonds work together in a synergistic way to 25 facilitate topology rearrangement. The relative increase or decrease in mobility of neighboring 26 chains, located around a specific dynamic bond within the polymer network, was investigated in 27 detail by adjusting the concentration of dynamic bonds and catalyst. The herein reported strategy 28 allows the production of dual dynamic polymer networks that exhibit much shorter relaxation 29 times and thus improved (re)processability in comparison to vitrimers with one type of dynamic 30 bond.

31 INTRODUCTION

32 Thermosets possess remarkable dimensional stability, stiffness, and chemical resistance.[1] 33 However, due to their permanent covalent cross-links, they are not suitable for recycling or 34 reshaping.[2] To overcome this limitation, researchers have been exploring reversible cross-35 linking strategies to introduce plasticity into thermosets, thus improving their recyclability.[3–7] 36 Since 2011, vitrimers have emerged as a promising class of dynamic materials that enable chain 37 mobility and plastic deformation through heat-driven chemical exchange of the constituting 38 covalent cross-links.[8-10] Unlike other reversible networks, vitrimers can facilitate material 39 flow by associating cross-links with reactive species, without undergoing complete dissociation 40 of their dynamic bonds.[11,12] The rate-limiting step of this macroscopic process is primarily 41 determined by the rate of a chemical reaction, provided that the diffusion of network components42 is fast enough.[13]

43 Given the obvious link with chemical reaction kinetics, it is not surprising that catalysis 44 has been an integral aspect of vitrimer research since its inception.[14–21] Since the seminal 45 work of Leibler and co-workers on Zn-catalyzed transesterification in epoxy-acid cured 46 vitrimers,[8] several dynamic covalent chemistries have been reported and are nicely 47 summarized in numerous comprehensive reviews.[22-24] Despite the increasing number of 48 chemical platforms, transesterification remains the most widely investigated vitrimer system 49 because of its ease of use and similarity to a type of conventional thermoset formulations. [25– 50 33]

51 While several strategies have been reported to control the dynamics of vitrimers, one 52 intriguing method is to rethink the design of the macromolecular architecture to promote 53 polymer chain diffusion and reactivity.[11,21] This can be achieved by altering the cross-link 54 density or introducing network defects to impact the intrinsic elasticity of vitrimers, thereby 55 improving their reprocessability.[34-38] Additionally, the availability of reactive species plays a 56 crucial role in the rate of macroscopic material flow.[12,39] To this end, depending on the 57 specific design choices, three general strategies can be distinguished: the targeted reduction in 58 dynamic bonds to control the density of reversible cross-links (Scheme 1a),[40-42] the dilution 59 of dynamic units, which involves the use of macromolecular non-reactive segments (Scheme 60 1b),[43,44] and the synergistic use of multiple dynamic motifs which has gained prominence 61 (Scheme 1c).[39,45-53] This latter strategy employs a combination of different reactive 62 chemistries to design materials with tailor-made viscoelastic profiles that can match user-defined 63 specifications.[54-56]

3



65 **Scheme 1.** The primary techniques utilized to manage the dynamics of vitrimers, exemplified for an epoxy-acid cured matrix.

Understanding and manipulating the criteria for true orthogonality or synergy between different dynamic cross-linkers remains an important challenge in the field.[57] At a shorter timescale, a dynamic bond may act as a "permanent linker" and put constraints on polymer chain diffusion, while at a longer timescale it may induce movement of polymer chains. The tendency for movement of neighboring polymer chains on a dynamic bond will have an important effect on the average relaxation rate of the overall polymer network.

Intrigued by the possibilities in creative macromolecular design, we herein studied the synergy of two dynamic covalent chemistries within epoxy-based vitrimers (**Scheme 2a**). Specifically, transesterification and siloxane exchange were intentionally chosen because both associative mechanisms involve hydroxyl groups, and are able to interact with the same basic organo-catalyst (*e.g.*, triazabicyclodecene or TBD, Scheme 2b). Moreover, we recently reported that siloxane bonds exhibit quite fast exchange properties when combined with TBD and hydroxyl groups.[20] Finally, the inherent stability and resistance of siloxane bonds to degradation and hydrolysis make siloxane-based materials highly desirable for a multitude of
industrial applications, including silicone elastomers and biomedical materials, for which
longevity and reliability are critical.[58]



84 Scheme 2. Design strategy for dual exchange vitrimers reported herein. a) Epoxy-acid curing using
 85 different functional monomers, and b) two synergetic associative dynamic covalent chemistries based on
 86 ester and siloxane exchange, catalyzed by the same basic catalyst TBD.

83

87 Adjusting the stoichiometry of the reactants or the catalyst loading may have an effect on 88 both chemistries, establishing their inherent synergy. To demonstrate this hypothesis, vitrimers 89 containing both esters and siloxane groups were synthesized using commercially available 90 compounds. The dynamic properties of these polymer networks, containing dual dynamic 91 groups, were analyzed using rheological experiments, and compared to reference materials 92 involving transesterification or siloxane exchange, individually. Additionally, different models 93 were utilized to differentiate and identify each reactive segment and characterize the exponential 94 decay of the stress relaxation behavior of the materials.[59] Importantly, in contrast to previously 95 reported crosslinked materials containing multiple dynamic groups, this approach enabled us to 96 reveal the origin of the rapid processability of the siloxane-ester materials and allow for tuning 97 material properties to cover a larger application scope. To demonstrate the versatility of the 98 proposed system, additional adjustments were made to the composition and amount of the 99 constituting components. These optimizations were aimed at achieving an optimal balance 90 between dynamicity and creep resistance.

101 EXPERIMENTAL

102 Chemicals. 1,5,7-Triazabicyclo[4.4.0]dec-5-ene (98%) (TBD), hexanoic acid (>99.5%) (HA)
103 and 1,2,7,8-diepoxyoctane (DiEpoxOct) were purchased from Sigma Aldrich (Merck). 1,3-Di(3104 glycidyloxypropyl)tetramethyldisiloxane (97%) (DiEPoxSilox) was purchased from Gelest, Inc.
105 4,4'-Methylenebis(*N*,*N*-diglycidylaniline) (TetraEpox) and 1,3-bis(aminomethyl)cyclohexane
106 (BA) were purchased from TCI. Sebacic acid (98%) (SA) was purchased from Acros Organics.

107 Instrumentation. Fourier-transform infrared spectroscopy (FTIR) spectra were recorded on a 108 Cary 630 FTIR Spectrometer by Agilent. Nuclear Magnetic Resonance (NMR) analyses were 109 conducted on a Bruker Avance 300 (300 MHz). The NMR spectra were measured in CDCl₃, and 110 chemical shifts (δ) are presented in parts per million (ppm), relative to CDCl₃ as the internal 111 standard. Differential Scanning Calorimetry (DSC) was performed with a Mettler Toledo 112 instrument 1/700. Typically, ~ 12 mg sample was placed in a sealed pan, flushed with nitrogen 113 gas and passed through a heat-cool-heat cycle at 10 °C/min in a temperature range of -100 °C to 114 100 °C. Three heat/cool cycles were done for each sample, where the last two cycles were 115 dedicated to analyzing the heat flow of the sample after being cooled in controlled 116 conditions. The T_g values recorded herein are those obtained from the third cycle.

117 Thermogravimetric Analysis (TGA) was measured with a TGA Q500 (TA Instruments). 118 Typically, ~2 mg of each sample was equilibrated at 50 °C for 30 min and was flushed with 119 nitrogen gas. All the experiments were performed with a heating rate of 10 °C/min up to 600 °C. 120 The reported values of $T_{d5\%}$ represent the temperature at which 5% of mass is lost. Isothermal 121 TGA was measured with a TGA Q500 (TA Instruments). Typically, ~5 mg of each sample was 122 equilibrated at 50 °C for 5 min and was flushed with nitrogen gas. For (siloxane-)ester and 123 siloxane-based substances, the tests involved heating up to 160°C and 220°C (the temperature 124 utilized during hot pressing), respectively. Subsequently, the temperature was maintained for 25 125 min for siloxane-ester, 40 min for ester, and 50 min for siloxane materials. Rheology 126 experiments were performed on an Anton Paar MCR 302. The experiments were performed in 127 parallel plate geometry using sample disks having a diameter of 8 mm and a thickness of about 2 128 mm. Stress-relaxation experiments were performed at different temperatures (200 to 150 °C, 129 with intervals of -10 °C) using a constant shear strain of 1% and a constant force of 1 N under 130 nitrogen. Each measuring step was preceded by a force normalization step of 1 N, while 131 monitoring the gap between each plate. Creep experiments at different temperatures (30-120 °C, 132 with intervals of +10 °C) were also performed using a constant force of 1 N. Additionally, in the 133 first 300 s no shear stress was applied. Following this, a 2000 Pa shear stress was applied for 134 5000 s, without recovery. Creep measurements were preceded by a time sweep measurement at 135 90 °C and fixed frequency of 1 Hz for 1 h to remove possible thermal history.

136 Synthesis of polymer networks (typical procedure).

Siloxane-containing networks (Scheme 3). The hardener (BA, 1,3bis(aminomethyl)cyclohexane) was added in a 20 mL cup, followed by TBD (5, 7.5, or 10 mol%
with respect to DiEPoxSilox). The compounds were mixed using a speedmixer® (DAC 150.1

FVZ) for 2 min at 3500 rpm. In a second step, 0.9 eq. (based on BA) of DiEpoxSilox was added and mixed at 3500 rpm in the speedmixer® until a homogeneous phase was obtained (approximately 30 sec). Finally, the resulting sample was heated to 50 °C for 14 h, then 60 °C for 14 h, before being post-cured at 85 °C in a vacuum oven for 24 h. The manufacturing process 14 employed 5 mol%, 7.5 mol%, and 10 mol% TBD, resulting in the samples being designated as 14 Am-1, Am-2, and Am-3, respectively (Scheme 3). These are the only samples within this study 14 that incorporate an amine (Am) hardener for their fabrication.



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Scheme 3. Synthesis of siloxane-based networks (Am-1, Am-2 and Am-3).

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Siloxane-ester networks (see Table 1 for ratios of each compound). The diepoxide molecule(s) (DiEpoxSilox or/and DiEpoxOct, Scheme 4) was (were) first placed in a 20 mL cup. Then, a certain amount of TBD catalyst was added to the cup, depending on the formulation being used. For all formulations of siloxane-ester networks reported in Table 1 (except TBD-5%), the same amount of catalyst was used, i.e., 68.83 mg of TBD catalyst. Only one sample (named as TBD-5% in Table 1), used 34.41 mg of TBD catalyst.

More precisely, the amount of catalyst used was chosen to correspond to 10 mol% catalyst (except for TBD-5%) with respect to sebacic acid (SA) (1 g) for the following formulations: TBD-10%, Sil-0%, Sil-25%, Sil-50%, and Sil-75% (Table 1). For acid content screening, the amount of TBD catalyst was kept constant at 68.83 mg to allow comparison, while the amount of acid content was varied. Specifically, the acid content was decreased from 1 g for 161 TBD-10% to 0.75 g for Ac-75%, then to 0.5 g for Ac-50%, and finally to 0.25 g for Ac-25%
162 (Table 1).

163 The compounds were stirred in a speedmixer® (DAC 150.1 FVZ) for 8 min (4 x 2min) 164 to form a clear solution and dissolve TBD, followed by TetraEpox. SA was then added to the prepared epoxide-TBD mixture and heated to 60 °C. The mixture was then left to stir vigorously 165 166 for 14 h at 60 °C. Thereafter, the temperature was increased to 80 °C and stirring was continued 167 until a clear, completely homogeneous mixture was obtained (approximately 2 h depending on 168 the reactant ratios). The resulting product was left to cure for a period of 6 h, then placed in a 169 vacuum oven at 110 °C for 16 h and then post-cured at 145 °C for 4 h. A series of samples were 170 produced with different epoxide/SA ratios (summarized in Table 1).



171



Scheme 4. Reactants and organo-catalyst used in the synthesis of siloxane-ester networks.



S	Sample label	Eq. ac.(SA)/ Eq. epox.	Total Epoxide Content (mol%)			T_{g} (°C) ^a	$\begin{array}{c} T_{\rm d5\%} \\ (^{\circ}\rm C)^{\rm b} \end{array}$	Swelling ratio (%) ^c	Soluble fraction
Screening			Tetra Epox	DiEpox Sil	DiEpox Oct				(%) ^c
Catalyst	TBD-5%	1/1	25	75	0	-34	237	342 ± 2	15.8 ± 0.2
loading	TBD-10%	1/1	25	75	0	-31	233	204 ± 4	8.7 ± 0.3
	Sil-0%	1/1	25	0	75	-5	280	168 ± 4	7.3 ± 0.9
Siloxane ^d	Sil-25%	1/1	25	18.75	56.25	-12	254	249 ± 2	17.3 ± 0.4
content	Sil-50%	1/1	25	37.5	37.5	-20	241	229 ± 8	11.9 ± 0.3
	Sil-75%	1/1	25	56.25	18.75	-25	233	280 ± 22	16.5 ± 0.3
A · 1	Ac-25%	0.25/1	25	75	0	-5	256	136 ± 5	1.9 ± 0.8
Acid	Ac-50%	0.5/1	25	75	0	-18	240	154 ± 3	4.2 ± 0.4
content	Ac-75%	0.75/1	25	75	0	-25	227	182 ± 7	6.2 ± 0.4

^a Glass transition temperature determined by DSC, third heating step, temperature ramp 10 °C/min. ^b TGA degradation temperatures at which 5 % ($T_{d5\%}$) mass loss was observed under nitrogen. ^b Swelling ratio and soluble

176 fraction were calculated by gravimetry. ^d The percentages in the sample label represent the proportion of DiEpoxSil 177 relative to the total amount of diepoxide molecules (DiEpoxSil and DiEpoxOct). The percentages in the sample label 178 indicate a decrease in the amount of SA from 1 g to 0.75 g (Ac-75%), 0.5 g (Ac-50%), and 0.25 g (Ac-25%) 179 respectively.

180

181 **Material reprocessing** (Figure S1, ESI). The polymer samples were cut into 1-mm-sized pieces 182 and placed in a two-part rectangular-shaped steel mold (30 mm \times 15 mm) for compression 183 molding. This assembly was placed for 2 min under a pressure of 1 metric ton in a hydraulic 184 press (hot press) that is preheated to 160 °C in the case of siloxane-ester materials and 220 °C for 185 siloxane networks. Then the pressure (by means of weight) was increased to 3 or 4 tons and held 186 constant for an additional time. The total pressing time ranged from 20 to 45 minutes, depending 187 on the material, with longer durations required for siloxane materials (45 min), followed by ester 188 (35 min) materials, then siloxane-ester materials (20 min). After completion of the pressing, the 189 mold was allowed to cool for 3-5 minutes before the sample was removed.

Swelling and soluble fraction analysis. The tests were performed on approximately 70-80 mg polymer samples at 25 °C in 6 mL THF. The swollen samples were removed after 3 days, wiped with a tissue, and swelling ratio was calculated as follows:

193 swelling ratio (%) = $\frac{m_s - m_i}{m_i}$, where m_s is the swollen mass and m_i is the initial mass.

In order to determine the soluble fraction, the materials were immersed in THF for a total of six days. To ensure accuracy of the measurement, the THF was replaced with a fresh batch (6 mL) after three days, which coincided with the time when the samples were taken to calculate the swelling degree. After 6 days, the solvent was removed, and the samples were dried under vacuum overnight at 50 °C. The soluble fraction was calculated as follows:

soluble fraction (%) = $\frac{m_i - m_d}{m_i}$, where m_d is the mass after drying and m_i is the initial mass.

200 RESULTS AND DISCUSSION

201 Since the physical properties and material flow tendency of vitrimers are determined by the rate 202 of chemical exchange reactions, we sought to investigate methods for controlling this rate. 203 Specifically, we examined the combination of siloxane and ester dynamic bonds within a single 204 vitrimer material, which are both responsive to the same catalyst (TBD). Our initial hypothesis 205 was that the rate of chemical exchange reactions could be modulated through the variation of 206 both siloxane and ester dynamic bond concentrations, as well as that of TBD, within the vitrimer 207 material. This, in turn, could result in notable alterations in the physical properties and material 208 flow characteristics of the produced vitrimers. To achieve this purpose, we prepared three 209 different series of networks, each focusing on a different aspect of the vitrimer: catalyst loading, 210 siloxane content, and ester content. The vitrimer materials were prepared by mixing the 211 diepoxide molecule(s) with TBD as the catalyst, TetraEpox as a cross-linker, and sebacic acid as 212 shown in Scheme 4. These monomers were readily accessible, allowing for efficient synthesis 213 and characterization of the dual dynamic networks. Moreover, TetraEpox was incorporated not 214 only as a crosslinker to promote network formation but also to impart an internal catalytic 215 function to the resulting structure. Indeed, the presence of tertiary nitrogen in crosslinkers, such 216 as TetraEpox, has been shown to facilitate transesterification without the need for an external 217 catalyst. For example, in a recent study, polyester vitrimers containing internal tertiary amine 218 moieties demonstrated efficient bond exchange as a result of internal catalysis provided by 219 tertiary amines, enhancing the recyclability and reshaping potential of vitrimers under mild 220 conditions.[60]

After the initial curing process, the mixture underwent an additional post-curing treatment (145 °C, 4 h) to promote network equilibration through transesterification reactions. This method resulted in vitrimer materials suitable for investigating the rate of chemical exchange reactions and their impact on physical properties and dynamic behavior. Two reference samples were also prepared: the first used the same procedure but substituted DiEpoxSilox with DiEpoxOct, resulting in an "only ester-based network". The second was composed solely of a siloxane-based network, as illustrated in Scheme 3, and Table S1 in the ESI. These reference systems enabled a comprehensive assessment of the contributions of siloxane and ester dynamic bonds to the properties of the vitrimer materials.

230

231 Monitoring network formation with FTIR

Fourier transform infrared spectroscopy (FTIR) was utilized to track the development of the network formation. The successful completion of the curing process was confirmed by observing the disappearance of the carboxylic acid stretching band of SA at 1684 cm⁻¹, and the appearance of an ester formation band at 1740 cm⁻¹ resulting from the reaction between the carboxylic and epoxide moieties (Figure S2, ESI). This reaction resulted also in the formation of a hydroxyl band at 3435 cm⁻¹. Furthermore, the complete elimination of the characteristic epoxide peaks of TetraEpox (972-890 cm⁻¹) and DiEpoxSilox (905 cm⁻¹) is evident in Figure S3 (ESI).

To gain more insights into the effect of TBD, DiEpoxSilox and hexanoic acid were reacted with and without TBD separately, and the reaction mixtures were analyzed by ¹H NMR (Figure S9, ESI). No additional reaction between the epoxide and acid groups was detected in the absence of TBD. On the other hand, the presence of TBD led to the formation of new peaks in the region 3.5-5.5 ppm, suggesting an addition reaction and/or anionic ring-opening polymerization (ROP) of epoxide moieties.[31] TBD was found to catalyze the addition reaction between the epoxide and acid groups, resulting in the creation of a polyhydroxy ester network.

Additionally, as illustrated in Figure 1, the formation of ether bonds via anionic ROP between 246 247 epoxide groups was identifiable through the observation of peak (4) at 1091 cm⁻¹. It is also 248 evident that the presence of siloxane groups had no significant impact on polyaddition compared 249 to ROP. Indeed, changing the ratios between DiEpoxSilox and DiEpoxOct mainly affected the 250 Si-CH₃ (3) and Si-O-Si (5) bands, which decreased considerably in the case of Sil-25% (Figure 251 1) and were not observed for a purely ester-based network (Sil-0%, Figure S8, ESI). On the other 252 hand, the amount of acid content had a significant impact on the network structure formed. For 253 instance, in the case of Ac-25%, the lowest acid content compared to the epoxide content (0.25:1) led to a notable increase in the peak (4) at 1091 cm⁻¹, indicating that anionic ROP was 254 255 the predominant mechanism, resulting in a predominantly polyether-based network. However, 256 increasing the acid content to 50% and 75% (Ac-25% and Ac-75%, respectively) decreased the 257 intensity of the peak that is correlated to polyether formation (Figure S5, ESI). In a similar 258 epoxy-acid system, it was suggested that etherification does not occur until the addition reaction 259 is complete.[31] This indicates that, in conditions of 1:1 stoichiometry, the ester formation is 260 predominant. Although other reactions, such as Fischer esterification of free hydroxyl and acids, 261 as well as transesterification of hydroxyl and ester bonds, could potentially occur,[31] FTIR 262 analysis did not detect any evidence of their formation. Specifically, a new ester peak 263 accompanied by the disappearance (or decrease) of the original ester peak was not observed.





265

Figure 1. FTIR spectral curves of TBD-10%, Sil-25% and Ac-25%.

267 Thermal analysis of vitrimers

268 The impact of chemical composition on the thermal properties of the polymer networks was also 269 studied. This was accomplished by analyzing the networks, reported in Table 1, using differential 270 scanning calorimetry (DSC) and thermogravimetric analysis (TGA) (Figure 2 and Table 1). The 271 results showed that decreasing the SA content resulted in an increase of the glass transition 272 temperature (T_g) (Figure S12, ESI) and the temperatures corresponding to a 5% weight loss 273 $(T_{d5\%})$ (Figure S16, ESI), which could be attributed to an increase in the proportion of the 274 crosslinked polyether segments in the network. Conversely, increasing the amount of DiEpoxSil 275 resulted in a decrease in T_g and $T_{d5\%}$ ranging from -5 to -31 °C (Figure S11, ESI) and 256 to 223 276 °C (Figure S15, ESI), respectively. In addition, the effect of the aliphatic chain length and the 277 type of the epoxide precursor (DiEpoxSil vs. DiEpoxOct) on the thermal properties was also 278 explored. A composition with a reduced fraction of DiEpoxSil, thereby increasing the fraction of 279 DiEpoxOct containing shorter carbon-carbon aliphatic chains, led to a more rigid network, 280 evidenced by the rise in T_g (from -25 to -5 °C) and $T_{d5\%}$ (233 to 280 °C). It is worth noting that 281 all samples analyzed in this study exhibited $T_{d5\%}$ values above 227 °C, far exceeding the 282 temperatures required for both ester transesterification and siloxane exchange. Additionally, the 283 thermal decomposition of the siloxane-ester networks can be distinguished by two stages: the 284 initial dissociation of esters and the subsequent decomposition of siloxane bonds (Figure S15-285 S17, ESI). The isothermal TGA experiments showed that a mass loss of approximately 1-3% was 286 recorded at 160°C after 20 min for (siloxane-)ester materials (Figure S19-S21, ESI).

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288



290 Swelling and soluble fraction analysis

Table 1 summarizes the outcome of the swelling experiments, which are consistent with the thermal analysis of the corresponding polymer networks. After solvent screening, THF was

293 selected as a solvent due to its compatibility with all monomers and the favorable swelling 294 behavior observed (swelling degrees between 130% and 340%). Despite being swollen in THF, 295 all samples were resistant to dissolution, indicating effective cross-linking and chemical bonding 296 among the polymer chains within the network. Increasing the catalyst amount from TBD-5% to 297 TBD-10% resulted in a decrease in the soluble fraction (from 16 to 9%), suggesting that a higher 298 cross-link density was favored by the additional presence of TBD. The soluble fraction decreased 299 further to 2% when the acid:epoxide ratio was reduced to 0.25:1 (Ac-25%). Additionally, this 300 network exhibited a decrease in its swelling ratio, which may be ascribed to an increased 301 crosslinking density and epoxy homopolymerization. The rigidity of the network structure played 302 also an important role in altering the outcome of swelling experiments. For example, 303 transitioning from a network of Sil-75% to one containing only DiEpoxOct (Sil-0%) resulted in a 304 respective decrease in swelling ratio and soluble fraction from 280% and 17% to 168% and 7%, 305 respectively. All these findings highlight the significance of regulating the reactant contents and 306 nature to achieve the desired network properties.

307 Viscoelastic characterization

308 To investigate the dynamic behavior of vitrimers containing dual dynamic groups, reported in 309 Table 1 and Table S1 (ESI), stress-relaxation experiments of single and dual dynamic vitrimers 310 were carried out across a wide temperature range of 150-200 °C (Figure S23-S27, ESI). An 311 initial basic calculation of the characteristic material stress relaxation time (τ^*) was based on the 312 time required for the initial stress or modulus to relax to 1/e of its value. The results revealed that 313 the dual dynamic network (TBD-10%) demonstrated dramatically shorter relaxation times in 314 comparison to the reference vitrimers (Sil-0% and Am-3, containing the same amount of 315 catalyst). At 200 °C, for example, the characteristic stress relaxation time of the dual dynamic 316 vitrimer was around 225 times faster than that of the "only siloxane-based" vitrimer (Am-3) and 317 about 24 times faster than that of the "only ester-based" vitrimer (Sil-0%) (Figure S28, ESI). 318 This suggests that the siloxane and ester dynamic bonds, catalyzed by TBD, work together in a 319 synergistic manner to facilitate topology rearrangement, in an extent that is greater than what 320 would be expected from the separate dynamic exchange chemistries.

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322

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Figure 3. Normalized stress-relaxation curves of TBD-10%, fitted to the double Maxwell model (a) and Arrhenius plots generated from the deconvoluted relaxation times of both modes (b), revealing an apparent activation energy of 82 ± 1 kJ/mol and 68 ± 1 kJ/mol for the fast and slow relaxation modes, respectively.

328

329 Because of the presence of two types of dynamic bonds, the stress-relaxation data were 330 subsequently analyzed via fitting with different models of exponential decay, namely, single 331 Maxwell model, stretched Maxwell model and double Maxwell model. While the single 332 Maxwell model did not provide a good fit for the stress-relaxation data of the benchmark 333 siloxane and ester networks, the stretched Maxwell model, on the other hand, could be 334 successfully applied (Figure S29 and Table S2, ESI). However, in the case of polymer networks 335 containing siloxane-ester dual dynamic chemistries (TBD-10%), the best fit was only obtained 336 using the double Maxwell model (Figure 3 and Table S3, ESI), which enables to take the two 337 different prominent modes of stress-relaxation into account. This observation provided a first 338 experimental support of the dual-dynamic relaxation behavior of the herein described vitrimers.

339 The deconvolution experiments of both segments shed light on the underlying 340 mechanisms governing the observed stress-relaxation behavior and highlight the efficacy of the 341 dual dynamic bonding approach in designing vitrimer materials with enhanced dynamic 342 properties. Specifically, deconvolution allowed to virtually separate the relaxation rate of the faster from the slower relaxing segments, which were attributed to transesterification ($E_a = 82 \pm$ 343 1 kJ/mol) and siloxane exchange ($E_a = 68 \pm 1$ kJ/mol), respectively (Figure 3b). Here, it was 344 345 rationalized that an already relaxed ester portion located in close proximity in space to a siloxane 346 bond, will considerably impact the relaxation rate of the dynamic siloxane bond. In particular, as 347 previously demonstrated for the relaxation behavior of blends of linear and star-shaped polymers,[61] a neighboring relaxed fraction will act as a "solvent" because it significantly 348 349 promotes diffusion. Higher temperatures resulted in faster relaxation rates and a more 350 pronounced "solvent" effect of the faster segments in dual-dynamic vitrimers.

351 The dynamic properties were controlled by adjusting the network composition and the 352 amount of catalyst used. The data indicated that the stress-relaxation of the siloxane-ester system 353 with 10 mol% TBD occurred about three times faster than the system with 5 mol% TBD (with 354 characteristic relaxation times τ^* of 3.3 s and 9.6 s, respectively, Fig. 4a). This is consistent with the "only siloxane-based" networks (Am-1, Am-2, and Am-3), which displayed a similar pattern, 355 356 where the material containing 10 mol% TBD had a 2.5 times faster stress relaxation than the material with 5 mol% TBD (with relaxation times of $\tau^* = 748$ s and $\tau^* = 1885$ s, respectively) 357 358 (Figure S30). These observations showed that higher catalyst loading could result in a larger 359 fraction of dynamic bonds (at a specific temperature) and therefore more efficient stress-360 relaxation.



361

Figure 4. Comparison of stress-relaxation times at 200 °C under varying catalyst loading (a) and acid content (b).

364

365 The relaxation behavior was also strongly influenced by the acid content. Vitrimers 366 prepared with a lower acid content exhibited slower relaxation behavior (Figure 4b). This 367 observation is consistent with the "solvent" effect of the faster segments discussed earlier. For 368 instance, the relaxation time of TBD-10% was found to be around 60 times faster than that of 369 Ac-25% ($\tau^* = 3.3$ s vs $\tau^* = 203$ s). Additionally, with a constant acid content in the vitrimers, the 370 siloxane content in the epoxy reactant emerged as an important factor influencing the relaxation 371 rate, as demonstrated in Figure 5. Specifically, as the siloxane content increased, the relaxation 372 time decreased accordingly, with the relaxation time of Sil-75%% being 6 times faster than that 373 of Sil-0% ($\tau^* = 14$ s and $\tau^* = 79$ s, respectively). Sil-25% sample exhibited a distinct behavior 374 with multiple relaxation profiles during the stress relaxation analysis (Figure 5). This can be 375 attributed to the relatively low siloxane content in Sil-25%, which plays a pivotal role for the 376 reprocessability. Unlike Sil-0% (no siloxane groups), and Sil-50%, Sil-75% and TBD-10%, 377 which have higher siloxane content, this difference in composition likely contributed to the 378 observed variability in relaxation rates across different time periods of Sil-25%.



379

Figure 5. Comparison of stress-relaxation times with varying siloxane content.

381

382 To evaluate the endurance of the fast characteristic relaxation time of TBD-catalyzed 383 materials through multiple mechanical recycling steps, the TBD-10% material was subjected 384 four times to compression molding at 160 °C. After each step, the resulting sample was analyzed 385 using FTIR, DSC, and TGA (Figure S6, S13 and S17, respectively). After undergoing recycling, 386 the materials exhibited a slight enhancement in thermal stability, as evidenced by a marginal 387 increase in the onset temperature of degradation ($T_{d50\%}$) from 405°C in the initial sample to 388 410°C in the recycled samples (R1-R4), ascribed to further crosslinking during the hot pressing process. Additionally, a stress-relaxation experiment was performed for the 4th cycle (Figure 389 390 S31). The average characteristic stress relaxation times of the materials are similar (between 3 391 and 6 seconds). The FTIR spectra, T_g and $T_{d5\%}$ values also exhibited a remarkable similarity. 392 These data confirm the effectiveness of TBD as a catalyst, even after multiple reprocessing 393 cycles.



Figure 6. Creep curves (shear strain as a function of time) of respectively TBD-10% (a), Sil-0% (b) and
 Am-3 (c) between 30 and 120 °C with an applied shear stress σ of 2 kPa for 5000 seconds.

397

398 It is important to determine the dynamic behavior both at a short and a longer timescale 399 to determine mechanical integrity as a function of time and temperature.[11] To that end, creep 400 experiments were conducted for TBD-10%, Sil-0%, and Am-3%. Specifically, a constant shear

401 stress of 2 kPa was applied for 5000 seconds between 30 °C and 120 °C, and the resulting strain 402 was measured over time (Figure 6). To practically verify whether the steady-state regime was 403 reached within the measured time-intervals, the creep compliance, J(t), was plotted as a function 404 of time.[12,62] In case of terminal relaxation (or steady-state flow), J(t) should exhibit a time 405 scaling of 1. However, in none of the tested materials such power law scaling could be achieved, 406 leaving out the possibility to derive meaningful creep rate (Figure S32, ESI).[63] The recorded 407 data further indicated that the single-component systems exhibited the highest creep resistance, 408 displaying purely instantaneous elastic deformation in which the creep compliance is dominated 409 by entropic elasticity effects (similar to thermoset materials).[9] In the case of the dual system 410 (TBD-10%), which showed the fastest stress-relaxation response, a higher creep sensitivity was 411 found. This material displayed early primary creep effects while reaching a power law scaling of 412 0.41 at 120 °C after 5000 s. These results highlight the synergistic effect of the two dynamic 413 bonds in the dual dynamic vitrimers, which not only resulted in faster stress relaxation but also 414 did not necessarily lead to a much faster creep response.

415 CONCLUSION

416 This study explored the synergistic impact of incorporating siloxane and ester dynamic bonds, 417 both catalyzed with TBD, into epoxy-acid cured vitrimers. The preparation of a series of 418 polyhydroxy ester networks containing siloxane moieties was achieved by adjusting the 419 concentration of (dynamic) bonds and catalyst loading. The resulting network structure was 420 found to be greatly influenced by the acid content used in the material fabrication process, with 421 lower acid content leading to a predominantly polyether-based network. These results 422 demonstrated that controlling dynamic bond concentration and catalysts in vitrimer materials can 423 effectively regulate the rate of chemical exchange reactions and enhance thermal and mechanical

424 properties. In addition, the dual dynamic networks displayed faster relaxation times than 425 vitrimers containing siloxane and ester groups individually, enabling faster topology 426 rearrangement.

427 ASSOCIATED CONTENT

428 Supporting Information. Containing Table S1 comprising the physical properties of Am-1,

429 Am-2 and Am-3, pictures of typical reprocessed materials, FTIR spectra, ¹H NMR of the model

430 reaction, DSC, TGA, stress-relaxation experiments and creep measurements.

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- 437 Notes
- 438 The authors declare no competing financial interest.

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